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# B1301\*

# INVESTIGATION OF 2-MW PEMFC POWER PLANT FOR HYDROGEN RECOVERY FROM CHLORINE INDUSTRY

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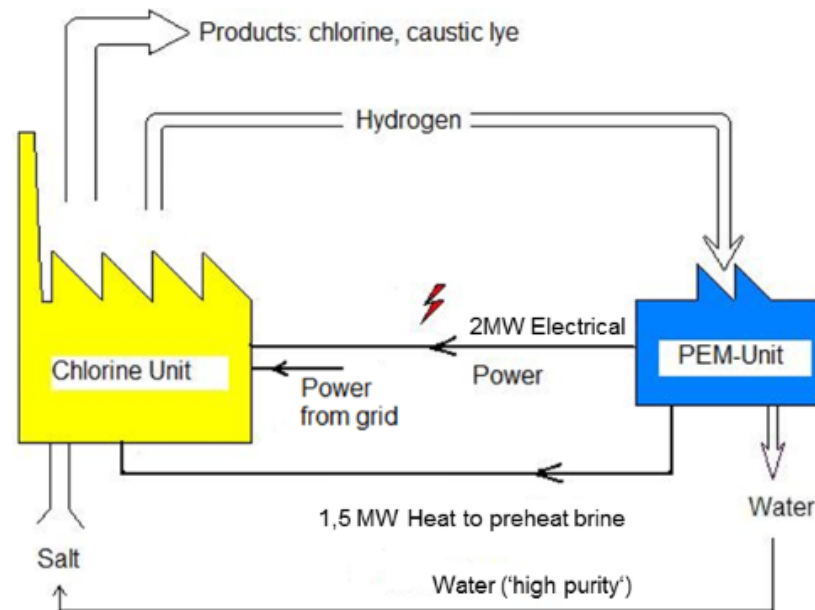
EFCE 2017 – 04-07 July 2017 – Lucerne (CH)

- ✓ DEMCOPEM-2MW PROJECT
- ✓ PLANT MODELLING
  - ✓ PLANT LAYOUT
  - ✓ MODELS VALIDATION
- ✓ PLANT OPERATION
  - ✓ REVERSIBLE-IRREVERSIBLE VOLTAGE DECAY
- ✓ CONCLUSIONS

Design, construction and demonstration of a combined heat and power (CHP) PEMFC power plant ( $2\text{MW}_{\text{DC el}}$ )

and

integration into a chlor-alkali industrial plant recovering byproduct hydrogen



## **OBJECTIVES (2015-2019)**

- **High net conversion efficiency** (> 50% electric and > 85% total)
- **Long lifetime** of system and fuel cells (16,000 h up to 40,000 h target)
- Development of large-volume **manufacturing process** for high-quality MEAs
- **Economical plant design** (< 2500 €/kW<sub>e</sub>)
- **Fully automated operation**
- Ensure plant reliability by developing protocols for **fuel cells monitoring and rapid replacement** of faulty stacks (on-stream availability of > 95%)
- Contribute to the general goals of the FCH-JU for installed fuel cell capacity

# PROJECT PARTNERS



**Johnson Matthey Fuel Cells**

*the power within*

High quality MEA assembly  
Manufacturing process  
development  
Performances, robustness,  
lifetime and costs optimization

**AkzoNobel**



Project coordinator  
Expertise in chlor-alkali plants



**Nedstack**

PEM FUEL CELLS

*To be sure.*

PEM fuel cell stack  
development and production



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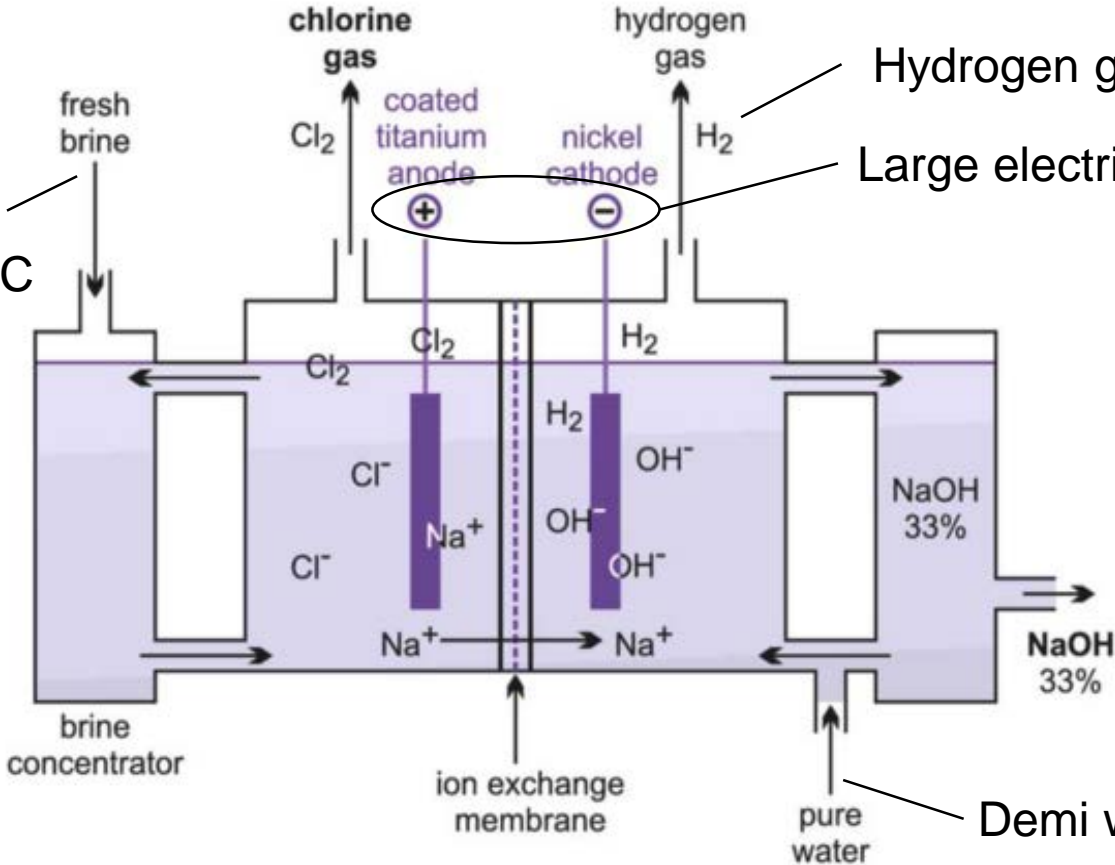
Power plant simulation  
model development,  
calibration and validation  
Analysis of experimental  
measurements

**INTSA**  
TECHNOPOWER

Development, production and  
maintenance of customer-  
specific equipment for energy  
processes

The Chlor-alkali process is suitable for integration with low temperature PEMFC:  
large need of heat and electricity

Reactants  
pre-heating:  
cells work at  
about 70-90°C



Hydrogen generated as byproduct  
Large electricity consumption (DC)

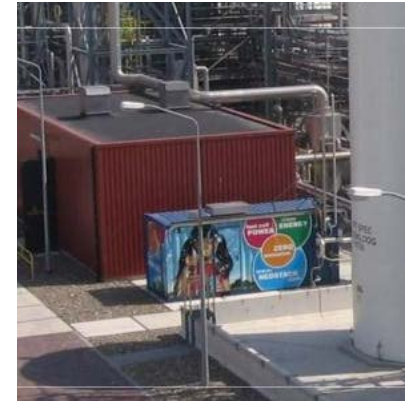
Demi water consumption

Installation is in **China**:

- high electricity price
- issues with supply shortages
- large chlor-alkali plants market - ca. 180 plants

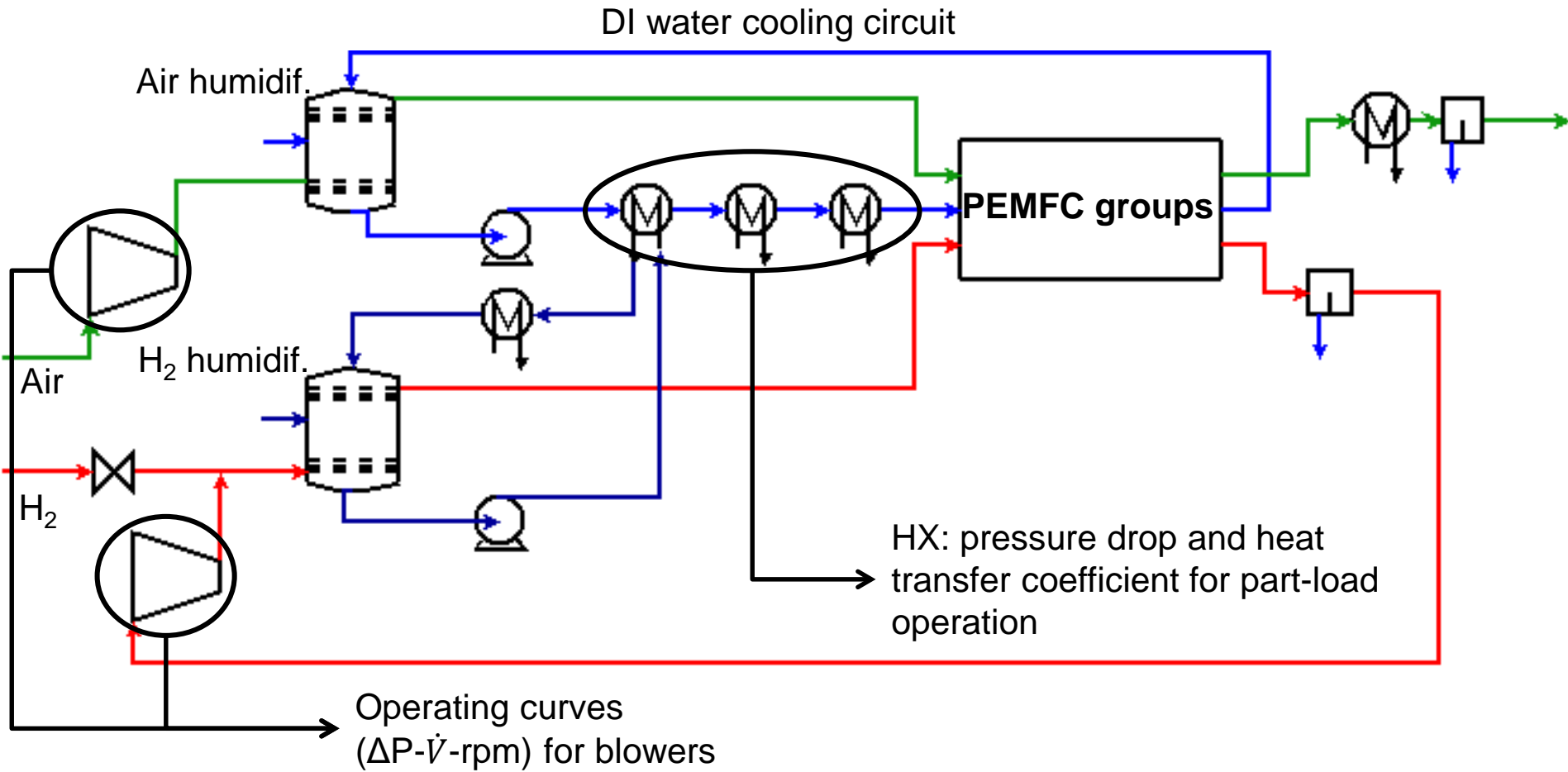
Scale-up based on previous experiences (Nedstack & MTSA)

- **70 kW<sub>el</sub>** PEM Power Plant at AkzoNobel (Delfzijl, NL, 2007)
- **1 MW<sub>el</sub>** PEM Power Plant at Solvay (Antwerp, BE, 2011)

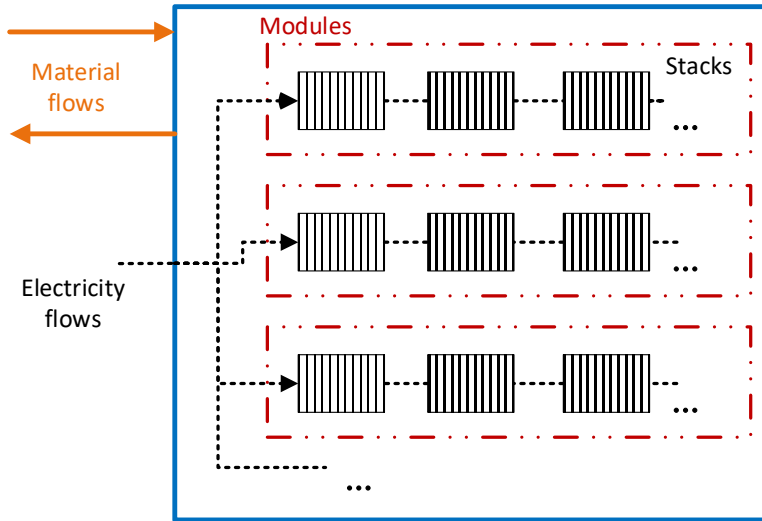




Model implemented in Aspen Plus, with custom models, for full- and part-load analysis



PEM Fuel Cell Model Block



Lumped model developed in Aspen Custom Modeler, for integration with the balance of plant is Aspen Plus

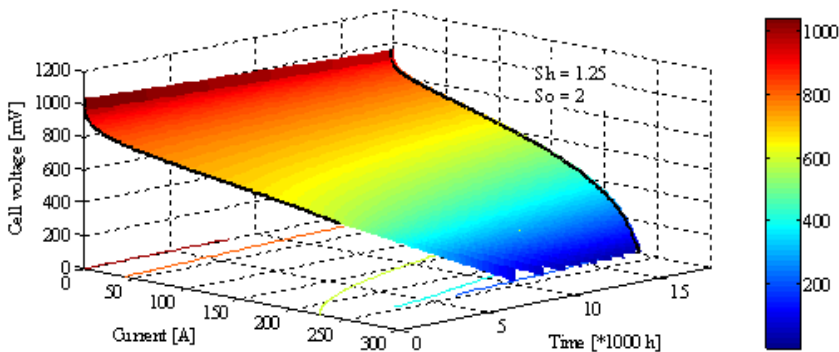
### Reflects the architecture of the plant:

Cells x 75 = Stack

Stacks x 14 = Module

Modules x 4 = Group

Groups x 6 = 2 MW power plant



### Empirical formulation of the i-V curve, validated against experimental data

Considers reactants stoichiometry ( $x_{H_2}$ ,  $x_{O_2}$ ), exchange and limit current density ( $i_0$ ,  $i_L$ ), linear long-period voltage decay ( $t_{BoL}$ - $t_{EoL}$ )

Neglects T and RH effects: stacks at constant T and RH thanks to the cooling water circuit and humidifiers

$$V(i, x_{H_2}, x_{O_2}) = \left[ A + B \ln \left( \frac{x_{H_2}}{x_{H_2,st}} \right) + C \ln \left( \frac{x_{O_2}}{x_{O_2,st}} \right) + Di + E \ln \left( \frac{i}{i_0} + 1 \right) + F \ln \left( 1 - \frac{i}{i_L} \right) \right] - G t(t_{BoL}, t_{EoL})$$



# PLANT OPERATION

**Construction and shipment** of the plant from M TSA factory (NL) to Ynnovate Ltd in Yingkou, Liaoning province, China



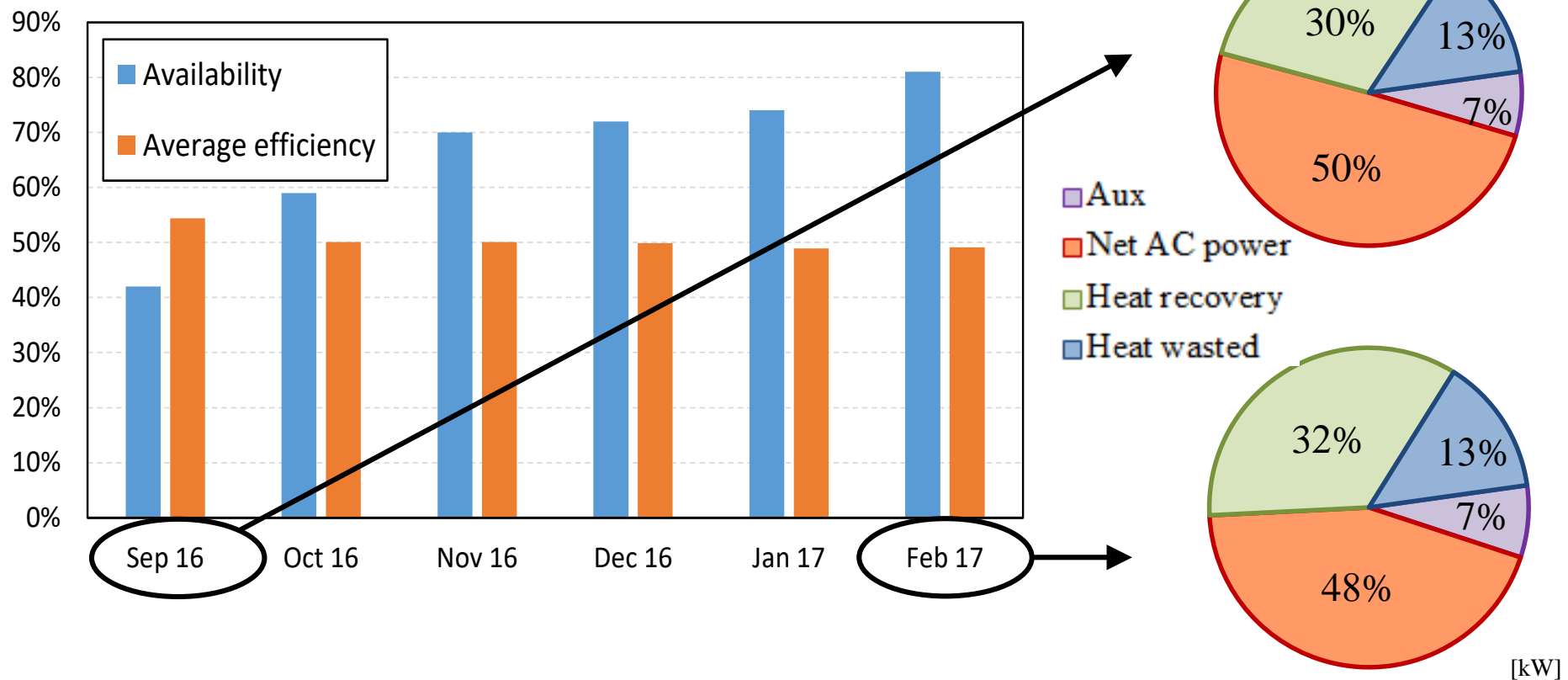
<https://www.youtube.com/watch?v=W8QE8iEXAyM>

**Opening ceremony** on 14 October 2016  
at plant location



Almost 10 months of plant operation:  
**data analysis**

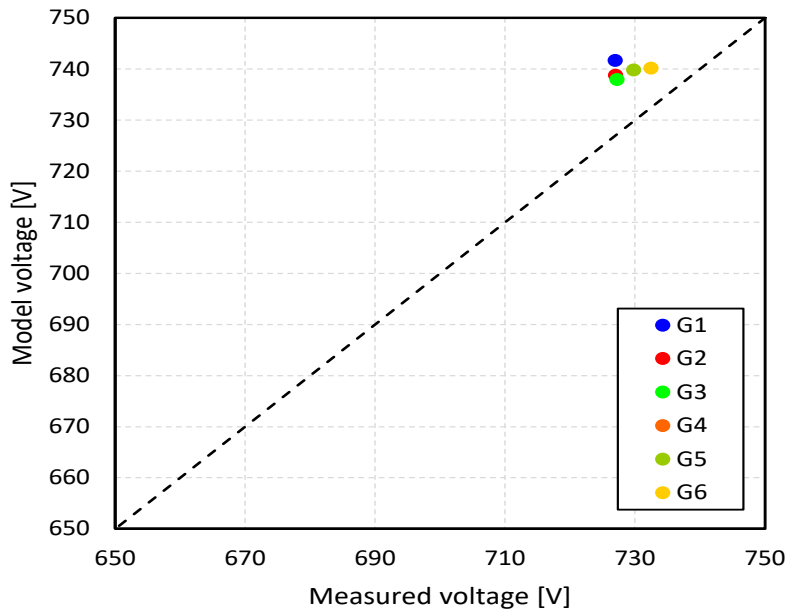




- Availability is increasing: main reason of low availability is **H<sub>2</sub> supply shortage** (and initial G4 inverter failure, now all the groups are available)
- **Net AC electric efficiency fulfills the 50% target** of the project, but decreases over time

The complete PEMFC power plant model is compared with field data

Voltage deviation at plant start-up



Property	Model-Measurements deviation [%]			
	15 Sep 16	19 Sep 16	19 Sep 16	13 Oct 16
Date	15 Sep 16	19 Sep 16	19 Sep 16	13 Oct 16
Active groups	5/6	4/6	3/6	5/6
Current [A]	-1.8%	-3.4%	-6.3%	-6%
Voltage [V]	+1.8%	+3.4%	+6.7%	+6.3%
Auxiliaries power [kW]	-1.2%	+9.7%	+8.9%	+6%
Coolant flowrate [m <sup>3</sup> /h]	-0.6%	-0.5%	-0%	+0.1%
Stack temp. [°C]	-1.3%	-1.4%	-1.1%	-2.6%

Very good agreement at Beginning of Life;  
 Poor agreement after 1 month of operation mainly due to change in operating conditions and decay: additional calibration performed.

# CONCLUSIONS & OUTLOOK

- Simulations of DEMCOPEM 2 MW power plant with a specific plant and PEMFC models
- The model is compared with field data: observed voltage overestimation by the model because does not account for reversible decay
- The plant fulfils the target net electric efficiency (50%) at Beginning of Life
- Plant operation was not continuous mainly because hydrogen shortage
- Voltage decay is observed in field conditions:
  - Reversible decay: fully recovered after corrective actions
  - Irreversible decay: calculation procedure under development

Next steps:

- Simulations: refine PEMFC models; continue data analysis
- Plant: implement strategies to limit the voltage decay



**Thank you for your  
attention!**

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